



Retorted Oil Shale In Estonia: An Environmental Audit

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Pollution is in the eyes of the beholder

Is it?

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Background



- 85 years of shale oil production
- two main processes today -
 - gaseous heat carrier, lumpy oil shale - semicoke
 - solid heat carrier, fine grained oil shale - coke-ash residue
- 80 years - ca 110 Million tons of spent shale (dw)
- semicoke - 2 bigger deposition areas
- coke-ash residue deposited together with combustion ash until today
- In last 5 years
 - ca 1 Million tons of semicoke and
 - 1 Million tons of coke-ash residue a year
- till the end of 20th century - “wet deposition method” of semicoke
- since then no extra water used besides water used for cooling the waste
- groundwater around the deposition areas is contaminated with phenols
- deposition areas to be reconstructed as landfills till 2009
- old deposition areas to be closed till 2013
- development of deposition technology - compaction of semicoke for better cementation

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Legal



Oil shale semicoke is classified as hazardous waste in the Estonian Waste List.

- The Waste List currently valid in Estonia is based on the EU Waste List.
- According to the general logic of the EU Waste List, wastes that have undergone the process of pyrolysis should be categorized as hazardous waste since they contain **tarry and bituminous substances**.

The solid waste of the solid heat carrier process has no separate number in the Estonian Waste List.

- It is still a pyrolysis waste.

Oil shale combustion ashes are also hazardous wastes.

All together 95% of the hazardous waste in Estonia



Legal II



Environmental impact of semicoke (investigation for Environmental ministry, 2003)

1. high TOC 12...14%
2. phenols
3. sulfides
4. bitumoids
5. high pH of leachates

Requirements for landfills

Waste acceptance criteria for landfills

TOC

- semicoke 8...14 (LHW limit 6%)
- coke-ash residue <1

Leaching limit values

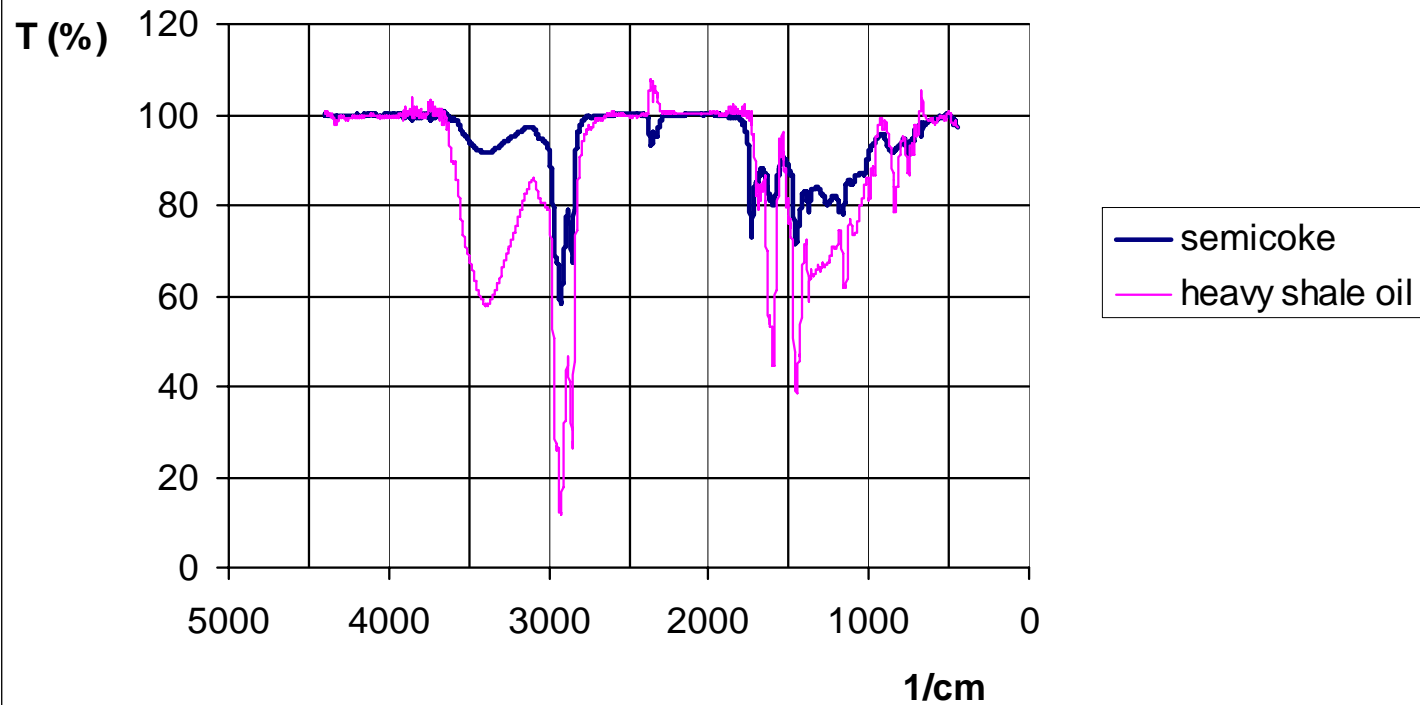
(DOC)



Bituminous substances



IR Spectra of semicoke soxhlet extract and heavy shale oil





TOC



| Parameter | Values | |
|-----------------------------------|--------|-----|
| | Min | Max |
| Fischer oil, % | <0,1 | 3,1 |
| Yield in Soxhlet extraction, g/kg | <1 | 16 |
| TOC, % | 8 | 11 |

***Most of TOC originates from pyrolysis char**

***Limit 6% (or less) can be achieved**

1) burning the char

2) using lower calorific value oil shale



LEACHING BEHAVIOUR OF OIL SHALE SEMICOKE



| Components | L/S = 10 l/kg | | | | L/S = 2 l/kg | | | |
|-------------------------------|------------------------------|---------|--------------------------------------|-----------|------------------------------|---------|--------------------------------------|-----------|
| | Leaching limit values, mg/kg | | Amount leached from semi-coke, mg/kg | | Leaching limit values, mg/kg | | Amount leached from semi-coke, mg/kg | |
| | Haz | Non-haz | Sample 25 | Sample 27 | Haz | Non-haz | Sample 25 | Sample 27 |
| Ca | - | - | 13000 | 9800 | - | - | 10000 | 1500 |
| Mg | - | - | 0.22 | 0.17 | - | - | 0.2 | nd |
| Fe | - | - | <0.2 | <0.2 | - | - | nd | <0.02 |
| Na | - | - | 150 | 230 | - | - | 118 | 190 |
| K | - | - | 550 | 1700 | - | - | 820 | 2700 |
| Al | - | - | 0.35 | <0.2 | - | - | 0.062 | 0.05 |
| As | 25 | 2 | <0.1 | <0.1 | 6 | 0.4 | nd | <0.1 |
| Ba | 300 | 100 | 1.7 | 3.1 | 100 | 30 | 1.8 | 1.3 |
| Cd | 5 | 1 | nd | nd | 3 | 0.6 | nd | nd |
| Cr (total) | 70 | 10 | <0.2 | <0.2 | 25 | 4 | nd | <0.02 |
| Cu | 100 | 50 | <0.2 | <0.2 | 50 | 25 | nd | nd |
| Hg | 2 | 0.2 | nd | nd | 0.5 | 0.05 | nd | nd |
| Mn | - | - | <0.2 | <0.2 | - | - | nd | <0.02 |
| Mo | 30 | 10 | 0.8 | 0.44 | 20 | 5 | 0.64 | 0.12 |
| Ni | 40 | 10 | <0.2 | <0.2 | 20 | 5 | nd | <0.02 |
| Pb | 50 | 10 | <0.2 | <0.2 | 25 | 5 | nd | <0.02 |
| Se | 7 | 0.5 | nd | <0.5 | 4 | 0.3 | nd | <0.05 |
| Zn | 200 | 50 | <0.2 | <0.2 | 90 | 25 | nd | nd |
| Sb | 5 | 0.7 | nd | <0.5 | 2 | 0.2 | nd | <0.05 |
| Sr | - | - | nd | 51 | - | - | nd | 35 |
| S _{total} | - | - | 11000 | 4600 | - | - | 11600 | nd |
| DOC | 1000 | 800 | 390 | 40 | 480 | 380 | 450 | 73 |
| SO ₄ ²⁻ | 50000 | 20000 | 740 | 860 | 25000 | 10000 | 260 | 150 |
| Cl ⁻ | 25000 | 15000 | 1800 | 2100 | 17000 | 10000 | 4600 | nd |
| F ⁻ | 500 | 150 | <5 | nd | 200 | 60 | nd | nd |
| TDS | 100000 | 60000 | 47500 | 32000 | 70000 | 40000 | 38000 | nd |

nd- not determined, elements that were not present in the solid semi-coke samples in amounts exceeding the leaching limits

“-“ no leaching limit values set



Oxidation of phenolics



1d/1w/8w



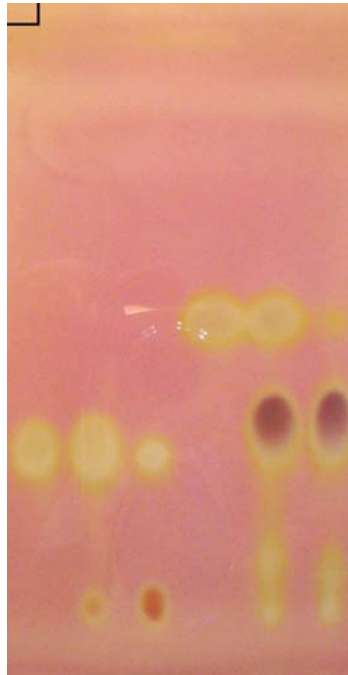
phenol+cresols

2,5 -dimethyl resorcinol

resorcinol+
5-methyl resorcinol

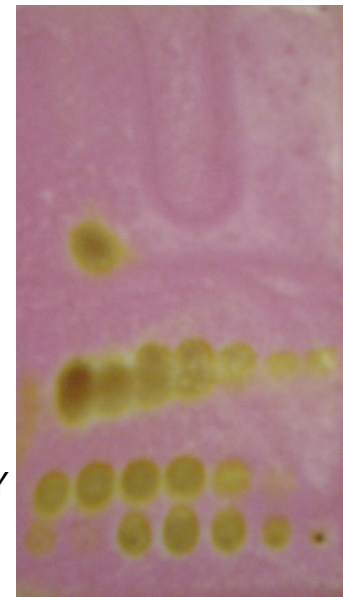
semicoke
leachate

0 2d 7d 0 1d 2d



5-methyl
resorcinol 2,5-dimethyl
resorcinol

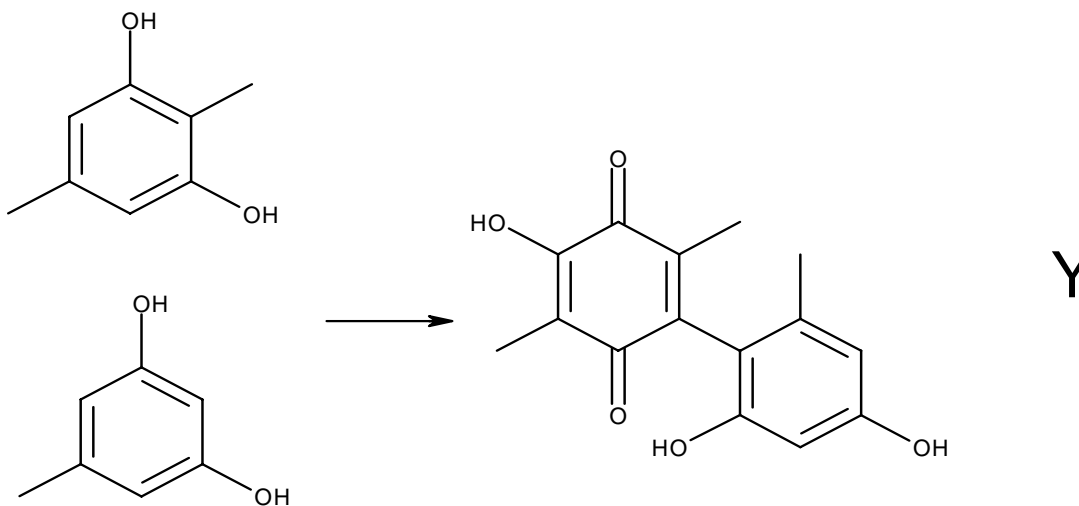
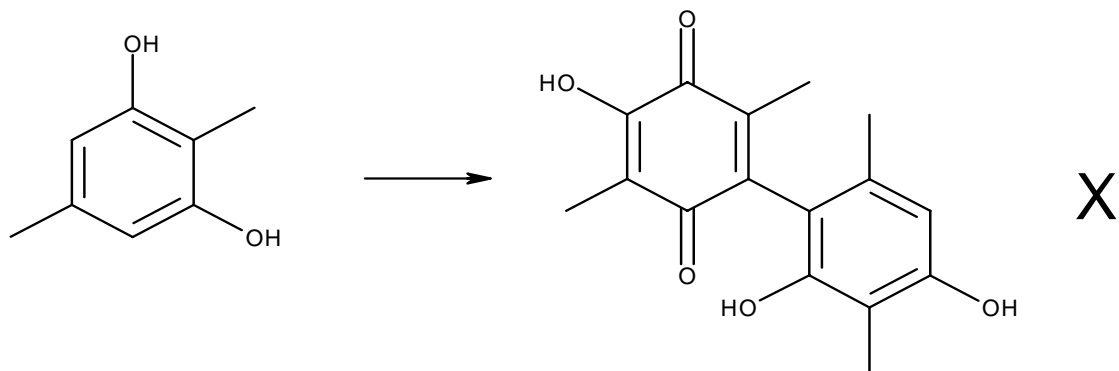
3h/1d/2d/4d/8d



5-methyl resorcinol +
2,5-dimethyl reorcinol

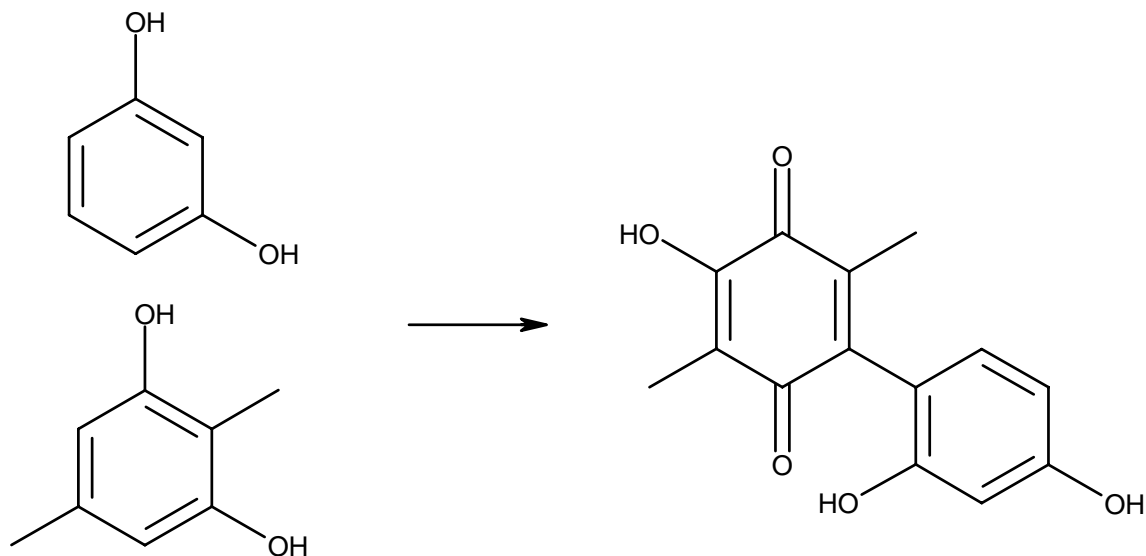


Oxidation of phenolics II





Oxidation of phenolics III



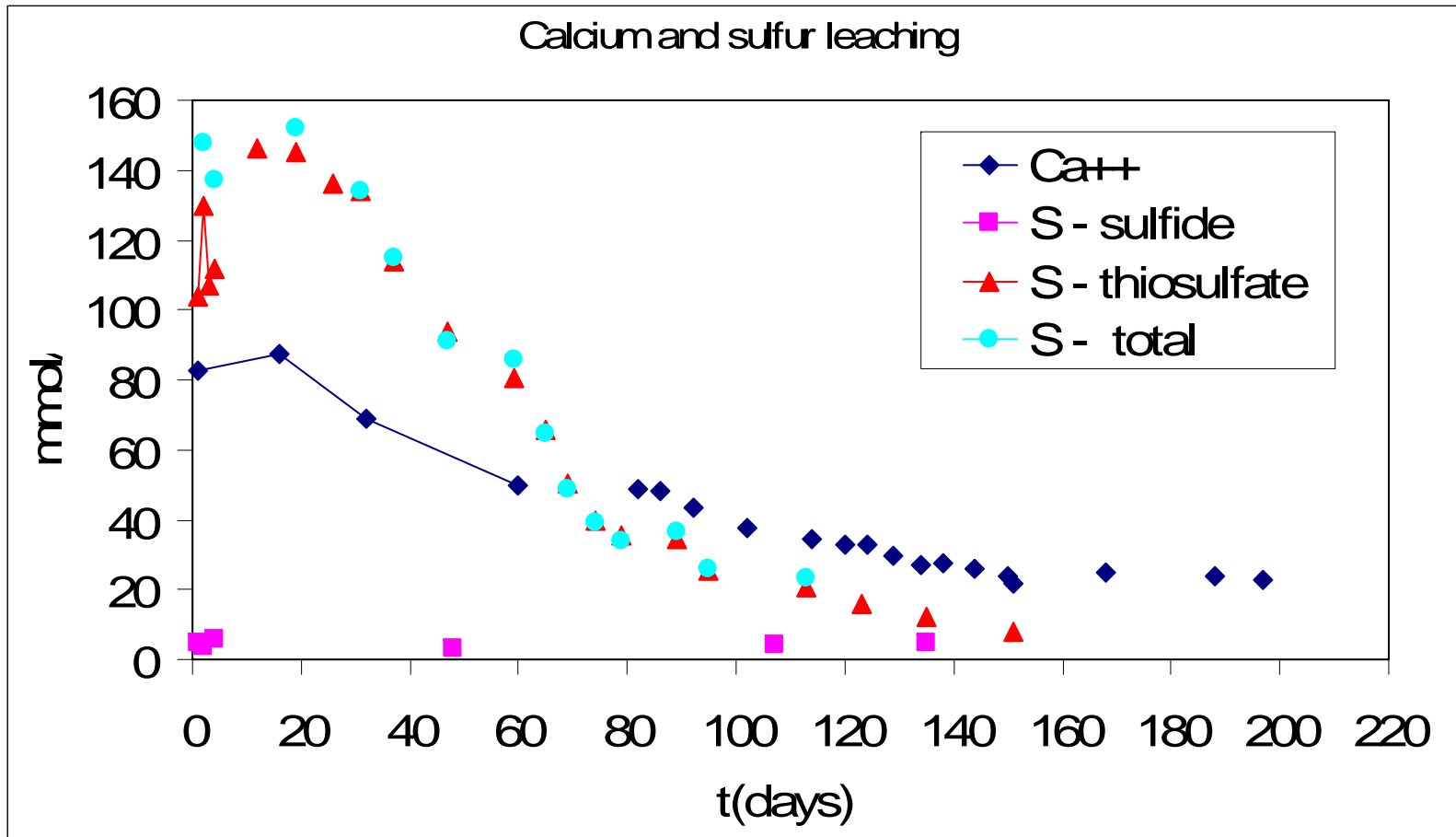
The reaction products shown are all stable intermediates



Leaching of sulfur species

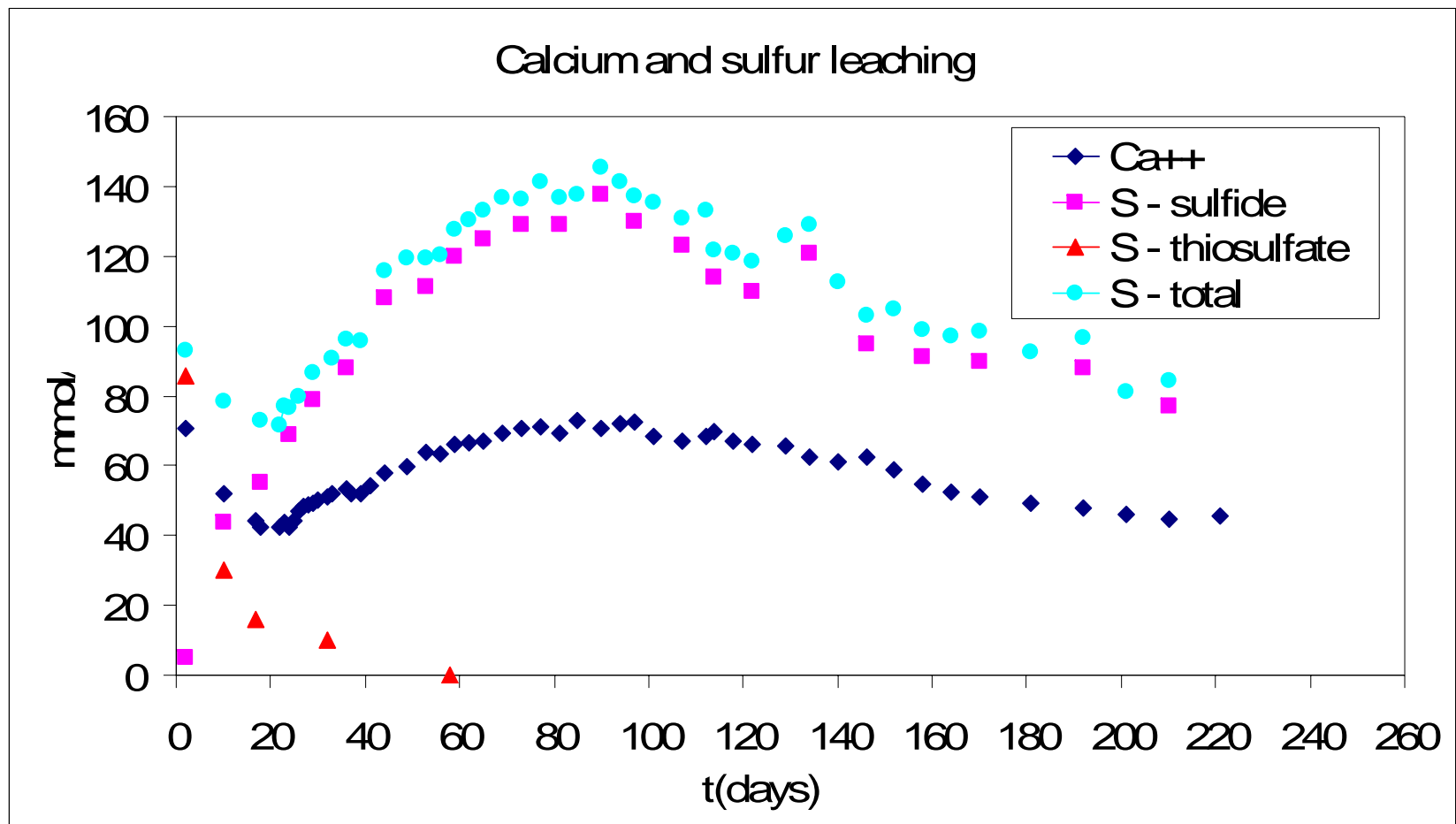


Total sulfur: 2...4%, sulfide sulfur 0,4...0,8%





Leaching of sulfur species II

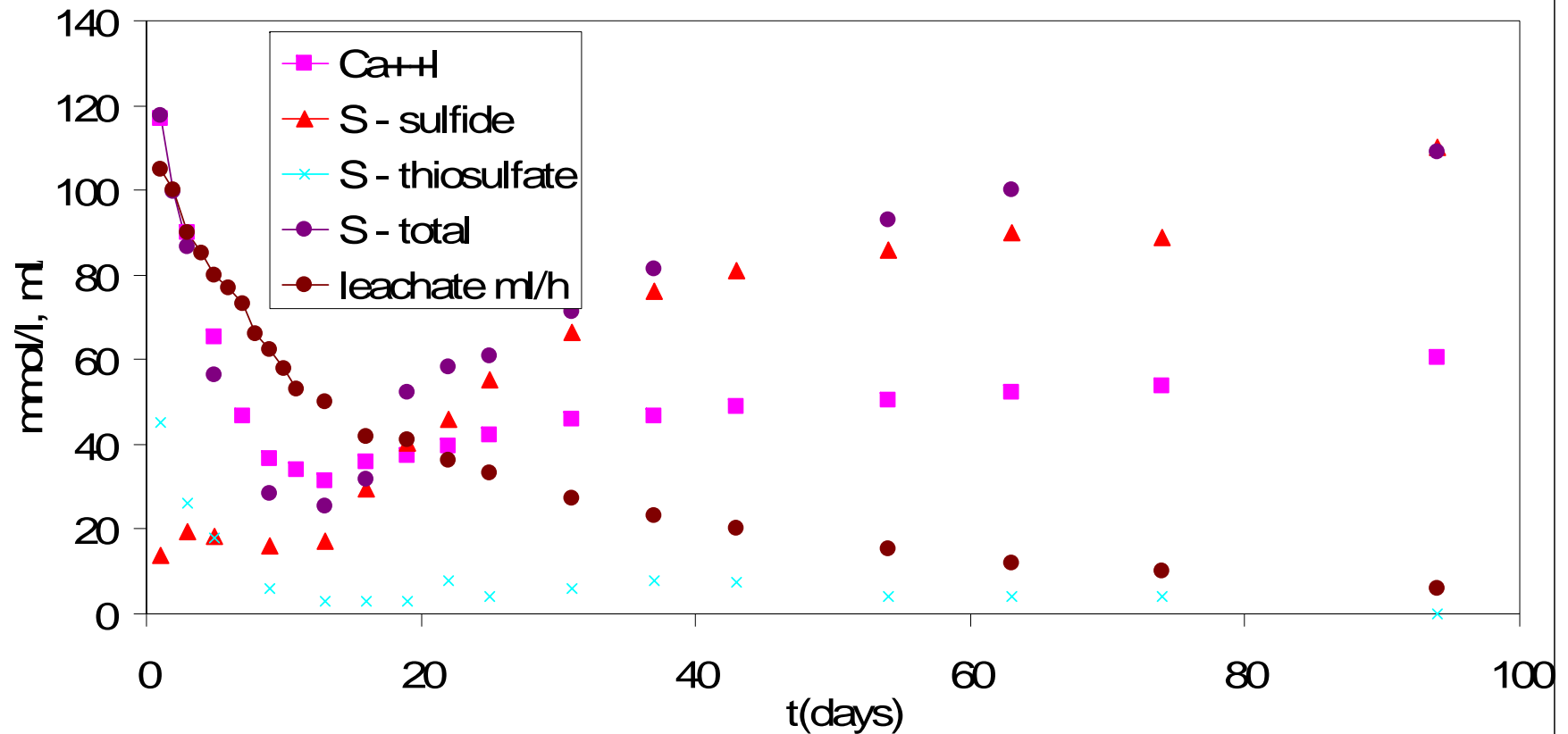




Leaching of sulfur species III



Calcium and sulfur leaching





Conclusions



A few words about sampling

No “new” extractable bituminous substances found

High TOC values do not reflect organic carbon

Phenols, if present, are oxidized

Sulfide leaching, hydrogen sulfide emission

High pH - possibilities of neutralization - P8



References

LEACHING BEHAVIOUR OF OIL SHALE SEMICOKE: COMPLIANCE WITH THE WASTE ACCEPTANCE CRITERIA FOR LANDFILLS Kaja Orupõld, Jaan Habicht, Toomas Tenno
Oil Shale, accepted

LEACHING BEHAVIOUR OF OIL SHALE SEMICOKE: SULPHUR SPECIES SPECIATION
Hedi Harzia, Kaja Orupõld, Jaan Habicht, Toomas Tenno, Oil Shale, accepted

Aknowledgements

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Thank you!

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